WE CLAIM:

- 1. A method of removing natural gas liquids from a gaseous natural gas stream at elevated pressure to produce a gaseous product stream having a reduced content of natural gas liquids, which method comprises the steps of:
- (a) cooling the natural gas stream;
- (b) introducing said cooled natural gas stream into the bottom of a scrub column that has a lower stripping section and an upper absorption section, each section containing at least one theoretical stage;
- (c) allowing natural gas to rise through the scrub column, and removing from the top of the scrub column an overhead stream;
- (d) partly condensing the overhead stream, and separating said partly condensed overhead stream into a gaseous stream having a reduced content of natural gas liquids and a liquid reflux stream, and removing the gaseous stream as the gaseous product stream having a reduced content of natural gas liquids;
- (e) splitting the liquid reflux stream into a first reflux stream and a second reflux stream:
- (f) introducing the first reflux stream into the top of the absorption section of the scrub column;
- (g) introducing the second reflux stream into the top of the stripping section to strip the desired light gaseous components; and
- (h) removing from the bottom of the scrub column a liquid bottom stream rich in heavier components.
- 2. The method of claim 1 wherein partly condensing the overhead stream in step (d) is cooled by indirect heat exchange with at least part of the gaseous product stream.

TS8585.DOC 18

- 3. The method of claim 1 further comprising introducing the liquid bottom stream at a lower pressure in the top of a stripping column having at least one theoretical separation stage; removing from the bottom of the stripping column a liquid stream of which a part is vaporized, which part is introduced into the bottom of the stripping column; removing from the top of the stripping column a gaseous overhead stream; partly condensing the gaseous overhead stream and separating the partly condensed overhead stream into a liquid fraction and a gaseous fraction; introducing the liquid fraction into the top of the stripping column; and adding the gaseous overhead fraction to the gaseous product stream.
- 4. The method of claim 3 wherein partly condensing the overhead stream in step (d) is cooled by indirect heat exchange with at least part of the gaseous product stream.
- 5. The method of claim 3 wherein the gaseous overhead is partly condensed by indirect heat exchange with the gaseous product stream.
- 6. The method of claim 4 wherein the gaseous overhead is partly condensed by indirect heat exchange with the gaseous product stream.
- 7. The method of claim 3 wherein the liquid bottom stream from the scrub column is cooled by indirect exchange with the gaseous product stream.
- 8. The method of claim 4 wherein the liquid bottom stream from the scrub column is cooled by indirect exchange with the gaseous product stream.
- 9. The method of claim 5 wherein the liquid bottom stream from the scrub column is cooled by indirect exchange with the gaseous product stream.
- 10. The method of claim 6 wherein the liquid bottom stream from the scrub column is cooled by indirect exchange with the gaseous product stream.

- 11. The method of claim 1 wherein the natural gas stream is partly condensed by indirect heat exchange with the gaseous product stream.
- 12. The method of claim 2 wherein the natural gas stream is partly condensed by indirect heat exchange with the gaseous product stream.
- 13. The method of claim 3 wherein the natural gas stream is partly condensed by indirect heat exchange with the gaseous product stream.
- 14. The method of claim 4 wherein the natural gas stream is partly condensed by indirect heat exchange with the gaseous product stream.
- 15. The method of claim 5 wherein the natural gas stream is partly condensed by indirect heat exchange with the gaseous product stream.
- 16. The method of claim 6 wherein the natural gas stream is partly condensed by indirect heat exchange with the gaseous product stream.
- 17. The method of claim 7 wherein the natural gas stream is partly condensed by indirect heat exchange with the gaseous product stream.
- 18. The method of claim 8 wherein the natural gas stream is partly condensed by indirect heat exchange with the gaseous product stream.
- 19. The method of claim 9 wherein the natural gas stream is partly condensed by indirect heat exchange with the gaseous product stream.
- 20. The method of claim 10 wherein the natural gas stream is partly condensed by indirect heat exchange with the gaseous product stream.
- 21. The method of claim 1 further comprising introducing hydrocarbon liquid into the top of the absorption section.
- 22. The method of claim 3 further comprising introducing hydrocarbon liquid into the top of the absorption section.

- 23. The method of claim 4 further comprising introducing hydrocarbon liquid into the top of the absorption section.
- 24. The method of claim 5 further comprising introducing hydrocarbon liquid into the top of the absorption section.
- 25. The method of claim 6 further comprising introducing hydrocarbon liquid into the top of the absorption section.
- 26. The method of claim 7 further comprising introducing hydrocarbon liquid into the top of the absorption section.
- 27. The method of claim 11 further comprising introducing hydrocarbon liquid into the top of the absorption section.
- 28. The method of claim 22 wherein the hydrocarbon liquid is cooled by indirect heat exchange with the gaseous overhead fraction.
- 29. The method of claim 23 wherein the hydrocarbon liquid is cooled by indirect heat exchange with the gaseous overhead fraction.
- 30. The method of claim 24 wherein the hydrocarbon liquid is cooled by indirect heat exchange with the gaseous overhead fraction.
- 31. The method of claim 25 wherein the hydrocarbon liquid is cooled by indirect heat exchange with the gaseous overhead fraction.
- 32. The method of claim 26 wherein the hydrocarbon liquid is cooled by indirect heat exchange with the gaseous overhead fraction.
- 33. The method of claim 27 wherein the hydrocarbon liquid is cooled by indirect heat exchange with the gaseous overhead fraction.